



ANALYSIS OF MULTIPHASE DISPERSIONS IN A STIRRED TANK USING A HIGH-PERFORMANCE RED LED LIGHT SOURCE PROBE

Alehlí Holguín-Salas, Gabriel Corkidi, Enrique Galindo; Departamento de Ingeniería Celular y Biocatálisis, Instituto de Biotecnología, Universidad Nacional Autónoma de México. Apdo. Postal 510-3, Cuernavaca, Morelos, C.P. 62250, México; email: alehli@ibt.unam.mx

Key words: Multiphase dispersion, image analysis, bubbles.

Introduction. In fermentations processes, an efficient dispersion of the gas phase is important to enhance the oxygen transfer phenomena. A diversity of techniques for analyzing gas dispersion exists and among these techniques, the image analysis has earned good acceptance in research and industrial areas by its feasibility and on-line acquisition of information. The main disadvantage of these techniques is the visual capability that is limited by the biomass concentration and the number of phases involved [1]. The aim of this work was to evaluate a commercial system, having high-performance illumination for *in situ* image acquisition and analysis, for studying multiphase dispersions.

Methods. The multiphase systems consisted in deionized water-air-biomass ($0.5 \text{ g}\cdot\text{L}^{-1}$), deionized water-air, and mineral media-air [2], at 1 vvm of air and 400 rpm ($0.27 \text{ W}\cdot\text{L}^{-1}$). The multiphase dispersion was analyzed in a stirred tank, 6.5 L of working volume, with a Rushton turbine ($D/T=0.33$), and the power drawn was determined using a dynamometer [2]. The zone analyzed was nearby the tank wall, between two baffles. It was used the commercial *in situ* probe image analysis system *EnviroCam*TM (Enviroptics, Colmar, PA, USA). The bubble Sauter diameter of 550 objects and the local gas fraction were analyzed with the *EnviroCam*TM software.

Results. It was possible to measure the Sauter mean diameter and the local gas fraction (in the case with two phases). The results obtained were compared with those reported by other authors [3,4] and that predicted with the following equation [5] (Table 1):

$$d_{32}/D = 8.5 \left(1 + 32.5 Q/D^2\right) \left(P_g/V\right)^{-0.24}$$

The *EnviroCam*TM system allowed to measure air bubbles with diameters as small as $30 \mu\text{m}$, as compared with $80 \mu\text{m}$ reported by Laakkonen *et al.* [3] in a conventional image system. This fact changes consequently the bubbles size distribution and therefore the mean Sauter diameter.

The illumination of the *EnviroCam*TM system allowed to obtain images with $0.5 \text{ g}\cdot\text{L}^{-1}$ of biomass (Fig. 1), a condition under which it is possible to clearly distinguish each dispersed phase for further analysis.

Table 1. Bubble Sauter diameter (d_{32} , μm) and local gas fraction (vol %), for an air-water dispersion.

	Bubble d_{32} (μm)	Gas (vol %)
This work ($0.27 \text{ W}\cdot\text{L}^{-1}$)	226 ± 29	19 ± 1.4
Predicted [5]	266	-
Falcón-Rojas [4] ($0.25 \text{ W}\cdot\text{L}^{-1}$)	180	-

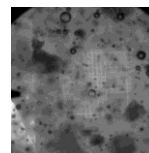


Fig. 1. Image captured with the *EnviroCam*TM using a three phases system (deionized water-air-biomass). In the image, a Neubauer chamber was placed in the background.

Conclusions. The improved illumination method of the *EnviroCam*TM, together with the high resolution (1024×1024 pixels) and the high acquisition rate (100 frames per second) allowed acquiring images of a three phases system. The phases were clearly distinguished, facilitating further analysis. Preliminary data of Sauter diameter were compared with previous data as well as with the valued predicted by a well accepted correlation, showing good agreement.

Acknowledgements. Financial support of the Instituto de Biotecnología-UNAM, and from CONACyT (grant 129676 and Alehlí Holguín Salas PhD scholarship 205247).

References.

- [1] Junker B, Maciejak W, Darnell B, Lester M, Pollack M. (2006). *Bioprocess Biosyst. Eng.* 29:185-206.
- [2] Galindo E, Larralde-Corona P, Brito T, Córdova-Aguilar MS, Taboada B, Vega-Alvarado L, Corkidi G. (2005). *J. Biotechnol.* 116(2):261-270.
- [3] Laakkonen M, Moilanen P, Alopaeus V, Aittamaa J. (2007). *Chem. Eng. Sci.* 62:721-740.
- [4] Falcón-Rojas A, Córdova-Aguilar MS, Galindo E. (2012). Effect of spatial position on the dispersion and interaction of oil drops and air bubbles in a three-phase system inside a stirred vessel. "Mixing XXIII" Meeting of the North American Mixing Forum, México, June 17-23, 2012.
- [5] Alves SS, Maia CI, Vasconcelos JMT, Serralheiro AJ (2002). *Chem. Eng. J.* 89:109-117.